

Fluid dynamics

• Thin film dewetting ($Re \ll 1$)



In previous lectures, we have discussed the shape of a sessile drop.

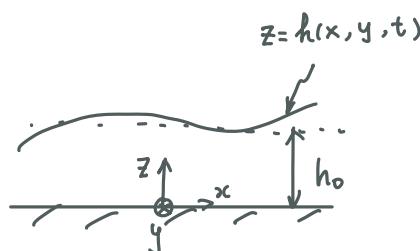
Now the questions arise for a thin film dewetting into drops: When / How / How fast?

- When does it occur?
- What is the characteristic size of the dewetting regions?
- How fast does it happen?

To answer these questions, first need a dynamics equation for h .

Kinematics

The surface satisfies $F(x, y, t) = z - h(x, y, t) = 0$



$$\frac{dF}{dt} = \frac{dz}{dt} \Big|_S - \underbrace{\frac{\partial h}{\partial x} \frac{dx}{dt} \Big|_S}_{w_s} - \underbrace{\frac{\partial h}{\partial y} \frac{dy}{dt} \Big|_S}_{v_s} - \frac{\partial h}{\partial t} = 0$$

$\frac{d}{dt} = \frac{\partial}{\partial t} + \underline{u} \cdot \nabla$ material derivative

$$w_s = \frac{\partial h}{\partial t} + u_s \frac{\partial h}{\partial x} + v_s \frac{\partial h}{\partial y}$$

kinematic boundary condition

Conservation of mass

Incompressibility : $\nabla \cdot \underline{u} = 0$, $\underline{u} = u \hat{e}_x + v \hat{e}_y + w \hat{e}_z$

$$\int_0^{h(x,y,t)} \nabla \cdot \underline{u} dz = \int_0^h \frac{\partial u}{\partial x} dz + \int_0^h \frac{\partial v}{\partial y} dz + \underbrace{\int_0^h \frac{\partial w}{\partial z} dz}_{= w_s - w(0)}$$

Recall Leibniz' theorem

$$\frac{\partial}{\partial x} \int_0^h u dz = \int_0^h \frac{\partial u}{\partial x} dz + u \frac{\partial h}{\partial x} \Big|_{z=h} = \int_0^h \frac{\partial u}{\partial x} dz + u_s \frac{\partial h}{\partial x}$$

Similarly, we have

$$\frac{\partial}{\partial y} \int_0^h v dz = \int_0^h \frac{\partial v}{\partial y} dz + v_s \frac{\partial h}{\partial y}$$

Combining these leads to

$$\frac{\partial}{\partial x} \int_0^h u dz - u_s \frac{\partial h}{\partial x} + \frac{\partial}{\partial y} \int_0^h v dz - v_s \frac{\partial h}{\partial y} + w_s = 0$$

Use the kinematic boundary condition to show

$$\frac{\partial h}{\partial t} + \frac{\partial}{\partial x} \int_0^h u dz + \frac{\partial}{\partial y} \int_0^h v dz = 0$$

Or

$$\boxed{\frac{\partial h}{\partial t} + \nabla \cdot \int_0^h \underline{u} dz = 0}$$

↑ Continuity condition.
flux Q

Conservation of momentum

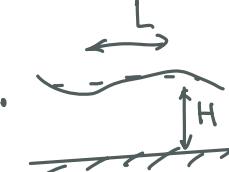
Navier-Stokes equation for an incompressible Newtonian viscous fluid.

$$\rho \frac{du}{dt} = \rho \left(\frac{\partial u}{\partial t} + u \cdot \nabla u \right) = -\underbrace{\nabla p}_{\text{Divergence of stress}} + \underbrace{\mu \nabla^2 u}_{\text{Diffusion}} + \rho g$$

Inertia

gravitational acceleration

Before proceeding, let us discuss the scaling due to the thin geometry.

-  $\Rightarrow \frac{\partial}{\partial x} \sim \frac{1}{L} \ll \frac{\partial}{\partial z} \sim \frac{1}{H} \rightarrow \epsilon = \frac{H}{L}$ (small parameter)

- $\nabla \cdot u = 0 \rightarrow u \sim v \sim \frac{W}{\epsilon}$

- $\rho(u \cdot \nabla u) \sim \rho u^2 / L, \mu \nabla^2 u \sim \mu u / H^2$. Inertia may be neglected

as long as $Re = \frac{\rho u L}{\mu} \times \frac{H^2}{L^2} = Re \cdot \epsilon^2 \ll 1$ (Reduced Reynolds number). Inertia

may be neglected even though Re is not that small.

We then consider the Stokes equations

$$\mu \left(\underbrace{\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2}}_{\epsilon^2 [u]/H^2} \right) - \frac{\partial p}{\partial x} = 0$$

$$\mu \left(\underbrace{\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2}}_{\epsilon^2 [v]/H^2} \right) - \frac{\partial p}{\partial y} = 0$$

$$\mu \left(\underbrace{\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2}}_{\epsilon^2 [w]/H^2} \right) - \frac{\partial p}{\partial z} + \rho g = 0$$

We focus on long-wavelength limit $\epsilon = \frac{H}{L} \ll 1$. The flow is mostly unidirectional (a.k.a.

(lubrication approximation)

$$\begin{cases} \mu \frac{\partial^2 \underline{u}}{\partial z^2} - \frac{\partial p}{\partial x} = 0 \\ \mu \frac{\partial^2 v}{\partial z^2} - \frac{\partial p}{\partial y} = 0 \quad \Rightarrow \quad \mu \frac{\partial u}{\partial z^2} - \nabla_s p = 0, \quad \underline{u} = u \underline{e}_x + v \underline{e}_y, \quad \nabla_s = \frac{\partial}{\partial x} \underline{e}_x + \frac{\partial}{\partial y} \underline{e}_y \\ \frac{\partial p}{\partial z} = \rho g \rightarrow p = \rho g (z - z_0) + f(x, y) \end{cases}$$

The pressure is approximately hydrostatic; The flow is quasi-parallel to the boundary

$$\underline{u}(z) = \frac{1}{2\mu} \nabla p z^2 + C_1 z + C_2$$

Boundary conditions:

$$\textcircled{1} \quad \underline{u}(0) = 0 \quad (\text{No-slip}) \rightarrow C_2 = 0$$

$$\textcircled{2} \quad \left. \frac{\partial \underline{u}}{\partial z} \right|_h = 0 \quad (\text{No-shear}) \rightarrow \underline{u}(z) = \frac{1}{2\mu} \nabla p (z^2 - 2zh)$$



$$\text{Flux across the thickness } Q = \int_0^h \underline{u}(z) dz = - \frac{h^3}{3\mu} \nabla p$$

Conservation of mass $\frac{\partial h}{\partial t} + \nabla \cdot \underline{Q} = 0$ gives

$$\frac{\partial h}{\partial t} = \frac{1}{3\mu} \nabla \cdot (h^3 \nabla p)$$

Reynold's equation.

Aside: What if ϵ is not that small?

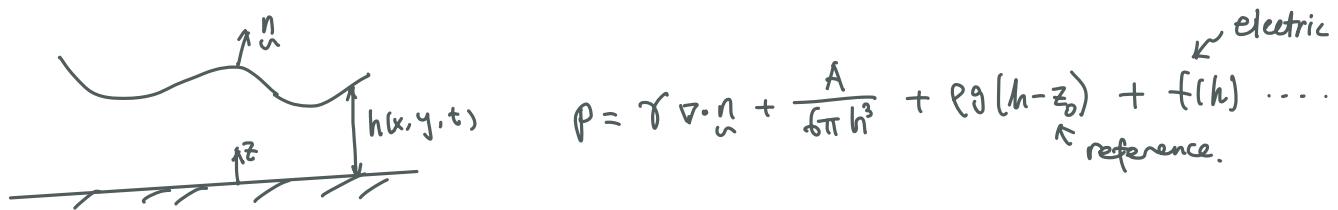
$$\underline{u}(\underline{x}, \epsilon) = \underline{u}_0(\underline{x}) + \epsilon^2 \underline{u}_2(\underline{x}) + \epsilon^4 \underline{u}_4(\underline{x}) + O(\epsilon^6)$$

$$w(\underline{x}, \epsilon) = w(\underline{x}) + \epsilon^2 w_2(\underline{x}) + \epsilon^4 w_4(\underline{x}) + O(\epsilon^6)$$

$$p(z, \epsilon) = p_0(z) + \epsilon^2 p_2(z) + \epsilon^4 p_4(z) + O(\epsilon^6)$$

Our focus has been on the leading order result $O(\epsilon^0)$

Typical source of pressure gradients



In particular, $\nabla \cdot n = \frac{\nabla F}{|\nabla F|} = \frac{-(h_{xx} + h_{yy})}{(1 + h_x^2 + h_y^2)^{3/2}} \approx -\nabla^2 h$ (Lubrication approximation)

$\nabla p = -\gamma \nabla (\nabla^2 h) - \frac{A}{2\pi h^4} \nabla h + \rho g \nabla h$

Constants point to γ , A , ρg .

1D thin film dewetting (Neglecting gravity)

$h(x, y, t) = h(x, t)$

$\frac{\partial h}{\partial t} = \frac{1}{3\mu} \frac{\partial}{\partial x} \left[h^3 \left(-\gamma \frac{\partial^3 h}{\partial x^3} - \frac{A}{2\pi h^4} \frac{\partial h}{\partial x} \right) \right]$

$= \frac{1}{3\mu} \frac{\partial}{\partial x} \left(-\gamma h^3 \frac{\partial^3 h}{\partial x^3} - \frac{A}{2\pi h} \frac{\partial h}{\partial x} \right)$

In statics, $\frac{\partial h}{\partial t} = 0$. In dynamics $\frac{\partial h}{\partial t} \neq 0$, whether a perturbation grows or decays?
(linear stability analysis)

Consider $h = h_0 + \eta(x, t)$, $\frac{|\eta|}{h_0} \ll 1$

$$\cdot \frac{\partial h}{\partial t} = \frac{\partial \eta}{\partial t}$$

$$\cdot h^3 = (h_0 + \eta)^3 = h_0^3 \left(1 + \frac{3\eta}{h_0} + \dots \right)$$

$$\cdot h^3 \frac{\partial^2 h}{\partial x^2} = h_0^3 \frac{\partial^2 \eta}{\partial x^2} + 3 \frac{\eta}{h_0} h_0^3 \frac{\partial^3 \eta}{\partial x^3}$$

$$\cdot \frac{1}{h} \frac{\partial h}{\partial x} = \frac{1}{h_0} \frac{\partial \eta}{\partial x} - \frac{\eta}{h_0} \frac{\partial \eta}{\partial x}$$

We obtain linearized form of governing equation

$$\frac{\partial \eta}{\partial t} = -\frac{\gamma h_0^3}{3\mu} \frac{\partial^4 \eta}{\partial x^4} - \frac{A}{6\pi\mu h_0} \frac{\partial^2 \eta}{\partial x^2}$$

Since this linearized equation has coefficients INdependent of x and t , seek

separable solution of form

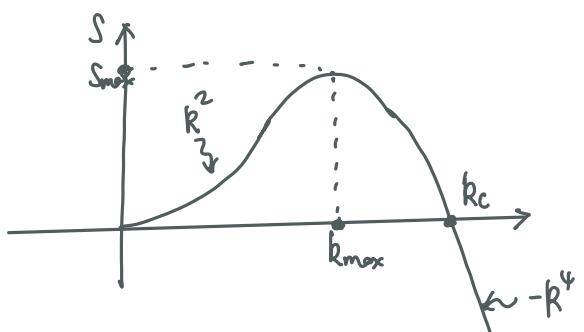
$$\eta = \eta_0 e^{st} e^{ikx}$$

wave number

so that the amplitude decays if $\operatorname{Re}(s) < 0$ and grows if $\operatorname{Re}(s) > 0$.

The characteristic equation is

$$s = -\frac{\gamma h_0^3}{3\mu} k^4 + \frac{A}{6\pi\mu h_0} k^2 \quad (\text{Always real number})$$



- $s > 0$ is possible if $A > 0$

- Surface tension stabilizes the system ($s < 0$)

- There is a fastest growing mode ($A > 0$)

* $S < 0$ for $R > R_c$

$$R_c = \left(\frac{A}{2\pi\gamma} \right)^{\frac{1}{2}} \frac{1}{h_0} \leftarrow \text{When to occur? Depends on } h_0 \text{ and system size } L.$$

* $\left. \frac{dS}{dR} \right|_{R_{\max}} = - \frac{4}{3} \frac{\gamma h_0^3}{\mu} R_{\max}^3 + \frac{A}{3\pi\mu h_0} R_{\max}^2 = 0$

$$R_{\max} = \left(\frac{A}{4\pi\gamma} \right)^{\frac{1}{2}} \frac{1}{h_0^2} = \frac{1}{\sqrt{2}} R_c$$

$$S_{\max} = \frac{A^2}{48\pi^2 \gamma \mu h_0^5}$$

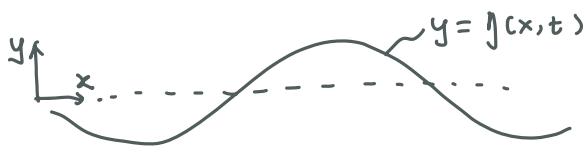
$$A = 10^{-20} \text{ J}, \gamma = 20 \text{ mJ/m}^2, h_0 = 100 \text{ nm} \rightarrow \lambda_{\max} = \frac{2\pi}{k} \approx 31.5 \text{ nm}$$

$$1000 \text{ nm} \rightarrow 31.5 \text{ mm}$$

$$10 \text{ } \mu\text{m} \rightarrow$$

$$3 \text{ m} \gg l_c$$

Capillary and gravity wave ($Re \gg 1$)



How y behaves?

$$F(x, y, t) = y - \eta(x, t)$$

Now consider a 2D inviscid flow with infinite depth

Kinematics

$$\frac{dF}{dt} = \frac{dy}{dt} - \frac{\partial y}{\partial x} \frac{dx}{dt} - \frac{\partial y}{\partial t} = 0 \quad (\text{on the surface})$$

\uparrow \uparrow
 v_s u_s

$$\rightarrow v_s = \frac{\partial y}{\partial t} + u_s \frac{\partial y}{\partial x} \quad \text{or} \quad v_s = \frac{\partial y}{\partial t} + \underline{u}_{ri} \nabla y$$

Continuity

$$\nabla \cdot \underline{u} = 0 \rightarrow \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

Momentum

$$\frac{d\underline{u}}{dt} = \frac{\partial \underline{u}}{\partial t} + \underline{u} \cdot \nabla \underline{u}$$

$$\rho \left(\frac{\partial \underline{u}}{\partial t} + \underline{u} \cdot \nabla \underline{u} \right) = -\nabla p_T + \rho g + \mu \nabla^2 \underline{u}$$

(Unsteady inviscid flows)
Euler equation, $M \rightarrow 0$

let $\rho = p_T + \rho g y$ and obtain

$$\rho \left(\frac{\partial \underline{u}}{\partial t} + \underline{u} \cdot \nabla \underline{u} \right) = -\nabla p \quad \text{dynamic pressure}$$

Linearization

Consider small amplitude so that g and \underline{u} are small, so is $\underline{u} \cdot \nabla \underline{u}$

We then have linearized governing equations:

$$\nabla \cdot \underline{u} = 0$$

$$\rho \frac{\partial \underline{u}}{\partial t} = -\nabla p$$

$$\nabla \left(\rho \frac{\partial \underline{u}}{\partial t} \right) = \rho \frac{\partial \nabla \cdot \underline{u}}{\partial t} = 0 = -\nabla^2 p$$

$$\rightarrow \nabla^2 p = 0$$

Assume $\hat{f}(x, t) = \hat{f} \exp[i k(x - ct)]$

$$= \hat{f} \exp[i(kx - \omega t)]$$

↑ Wavenumber ↑ Frequency
 $k = \frac{2\pi}{\lambda}$ $\omega = \frac{\omega}{k}$

Then natural to assume

It's like taking
 $s = -i\omega t$ - Never
decay !! It's fine to
be wrong, then we
will end up with a
Complex ω

$$P(x, y, t) = \hat{P}(y) \exp[i(kx - \omega t)]$$

\nwarrow
 \uparrow

The simplest guess - base pressure difference is more interesting
in y direction than x direction!

$$\nabla^2 P = \frac{\partial^2 P}{\partial x^2} + \frac{\partial^2 P}{\partial y^2} = \left(-k^2 \hat{P} + \frac{d^2 \hat{P}}{dy^2} \right) \exp[i(kx - \omega t)] = 0$$

$\underbrace{\quad}_{=0}$

The solution is $\hat{P} = A e^{-ky} + B e^{ky}$

($\text{Infinity} \rightarrow 0$ since $\hat{P} = \hat{P}_T + \rho g y$ already considered gravity)

$$\rightarrow P = B e^{ky} e^{i(kx - \omega t)} + \text{Any constants (e.g. Patm)}$$

Now back to the momentum equation (dynamic boundary condition)

$$\rho \frac{\partial u}{\partial t} = -\nabla P \rightarrow \rho \frac{\partial v}{\partial t} = -B k e^{ky} e^{i(kx - \omega t)}$$

$$v = \frac{-i B k}{\rho \omega} e^{ky} e^{i(kx - \omega t)}$$

$$\text{Kinematic B.C.} \rightarrow v_s = \frac{\partial y}{\partial t} + D(y) = -i \omega \hat{j} e^{i(kx - \omega t)} \quad (\text{On the surface})$$

We then have

$$w \hat{j} = \frac{B k}{\rho \omega} e^{ky} \Big|_{y=0} = \frac{B k}{\rho \omega} (1 + ky + \dots)$$

Neglect this to be consistent.

$$\Rightarrow B = \frac{\rho \omega^2 \hat{j}}{k}$$

This is not done since \hat{j} remains unknown.

We haven't used pressure jump condition on the surface (stress b.c.)

$$\sigma_{xx} = -\frac{\partial^2 y}{\partial x^2}$$

$$P_T = P_{atm} + \gamma \nabla \cdot \hat{n} = P(y=j) - \rho g j$$

$$\rightarrow \gamma \hat{j} k^2 e^{i(kx-wt)} = 8 \rho \hat{j} e^{i(kx-wt)} - \rho g \hat{j} e^{i(kx-wt)}$$

$$\rightarrow \frac{\gamma \hat{j}}{k^2} = \frac{\rho w^2 \hat{j}}{k} - \rho g \hat{j} \quad (\hat{j} \text{ does not matter - linearization is successful})$$

We finally have

$$\omega = \left(\frac{\gamma k^3}{\rho} + g k \right)^{1/2} \quad \leftarrow \text{Dispersion relation} \quad \text{色散関係}$$

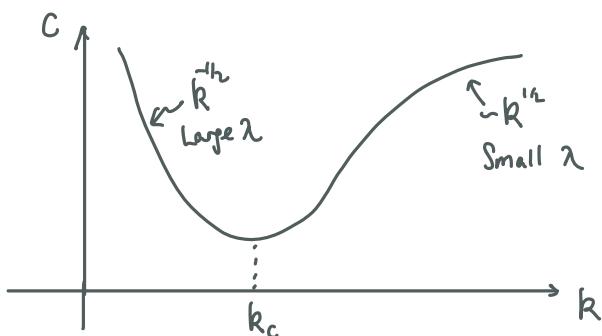
A wave is called dispersive since its different Fourier components disperse / disperse.

and

$$c = \left(\frac{\gamma k}{\rho} + \frac{g}{k} \right)^{1/2} \quad \leftarrow \begin{aligned} &\text{In a dispersive system, the energy} \\ &\text{propagates at the group speed } c_g = \frac{dc}{dk} \end{aligned}$$

$$\text{instead of phase speed } c = \frac{\omega}{k}$$

Observations



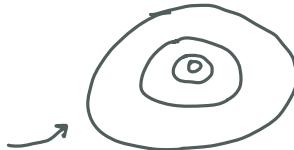
① Relative importance of γ and g is described by Bond number

$$Bo = \frac{\rho g}{\gamma k^2} = \frac{\rho g \lambda^2}{4\pi^2 \gamma} . \quad \text{For air-water, } Bo \approx 1 \text{ for } \lambda = 2\pi k \approx 1.7 \text{ cm}$$

② $Bo \gg 1$ as $\lambda \gg 2\pi k$: Surface tension effect negligible \Rightarrow Gravity wave

$$C \approx (g/k)^{1/2} = (g\lambda/2\pi)^{1/2}$$

Longer waves travel faster



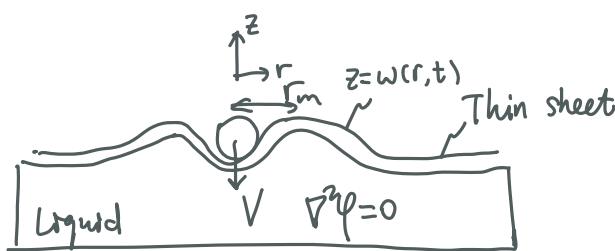
③ $Bo \ll 1$ as $\lambda \ll 2\pi l_c$: Influence of g negligible \Rightarrow Capillary wave

$$C \approx (\gamma k/\rho)^{1/2} = (2\pi\gamma/\rho\lambda)^{1/2}$$



Short waves travel fastest!

Elasto-capillary waves



Inviscid, incompressible, irrotational.

Now take $\underline{u} = \nabla \psi$ \leftarrow velocity potential

- Incompressibility $\nabla \cdot \underline{u} = 0$, requiring

$$\nabla^2 \psi = 0$$

• Kinematic condition $\frac{\partial \psi}{\partial z} = \frac{u_z}{\partial t} + \frac{\partial \psi}{\partial r} \frac{\partial w}{\partial r}$

- Dynamic boundary condition

$$\rho \left(\frac{\partial \underline{u}}{\partial t} + \underline{u} \cdot \nabla \underline{u} \right) = -\nabla p + \rho g \rightarrow \nabla \left[\rho \frac{\partial \phi}{\partial t} + \frac{1}{2} \rho |\nabla \psi|^2 + p - \rho g z \right] = 0$$

$$= \frac{1}{2} \nabla \left[\underline{u}^2 - \underline{u} \times (\underline{\omega} \times \underline{u}) \right]$$

Irrational flow

$$\rightarrow \rho \frac{\partial \phi}{\partial t} + \frac{1}{2} \rho |\nabla \psi|^2 + p - \rho g = f(u)$$

(Bernoulli's equation)

- Stress boundary condition

① Capillary force only $P = -\gamma \left(\frac{\partial^2 w}{\partial r^2} + \frac{1}{r} \frac{\partial w}{\partial r} \right)$

② Membrane force only $P = -N_{rr} \frac{\partial^2 w}{\partial r^2} - N_{\theta\theta} \frac{1}{r} \frac{\partial w}{\partial r}$



$$N_{rr} - dN_{rr} \quad \frac{\partial N_{rr}}{\partial r} + \frac{N_{rr} - N_{\theta\theta}}{r} = 0$$

Relaxed membrane $N_{\theta\theta} \ll N_{rr} \rightarrow N_{rr} = \frac{c}{r} = \frac{\sigma R_f}{F} \quad \left(\epsilon_{rr} - \frac{N_{rr}}{\gamma} = \frac{\sigma R_f}{\gamma r} \sim 10^{-4} \right)$

Tensioned membrane $N_{rr} \sim \gamma \epsilon_{rr} \sim \gamma \cdot \left(\frac{\rho R_s V^2}{\gamma} \right)^{1/3} \quad \left(\epsilon_{rr} \sim W_e^{1/3} \sim 1 \right)$

- Scaling point of view

Mass: $\nabla^2 \psi = 0 \rightarrow z_* \sim r_m$ (The base feels the r_m in the way it feels z_*)

Momentum: $\psi_* \sim V \times z_* \sim V \times r_m$

Stress: $\rho \frac{\psi_*}{t} \sim P \sim \begin{cases} \gamma \frac{Vt}{r_m^2} \text{ (capillary force)} \rightarrow \psi_* \sim \frac{\gamma V t^2}{\rho r_m^2} \\ \frac{\sigma R_f}{r_m} \frac{Vt}{r_m^2} \text{ (Relaxed membrane)} \rightarrow \psi_* \sim \frac{\sigma R_f V t^2}{\rho r_m^3} \\ \gamma W_e^{1/3} \frac{Vt}{r_m^2} \text{ (Tensioned membrane)} \rightarrow \psi_* \sim \frac{\gamma W_e^{1/3} V t^2}{\rho r_m^2} \end{cases}$

$$\Rightarrow \begin{cases} \text{Inertia-Capillary: } r_m \sim \left(\frac{V}{\rho} \right)^{1/3} t^{2/3} \\ \text{Inertia-elasto-Capillary (Relaxed): } r_m \sim \left(\frac{\sigma R_f}{\rho} \right)^{1/4} t^{1/2} \\ \text{Inertia-elasto-Capillary (Tensioned): } r_m \sim \left(\frac{\gamma}{\rho} \right)^{1/3} \left(\frac{\rho R_s V^2}{\gamma} \right)^{1/9} t^{2/3} \end{cases}$$