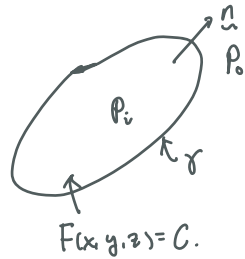


Fluid Statics

In last lecture, we discussed the pressure jump across an interface,

i.e., Laplace's theorem

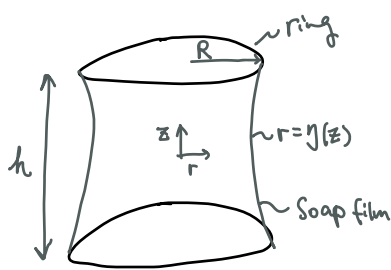


$$\Delta P = P_i - P_o = \gamma \nabla \cdot \underline{n}, \text{ where } \underline{n} = \frac{\nabla F}{|\nabla F|}$$

In this lecture, we discuss a number of examples, some of which

can lead to the measurement of surface tension of liquids.

• Minimal surfaces (Plateau's problem raised by Lagrange in 1760)



Determine $g(z)$?

The pressure jump has to be zero:

$$P_{atm} = P_{atm} + \underbrace{\gamma \nabla \cdot \underline{n}}_{P_i} + \gamma \nabla \cdot \underline{n}$$

This problem becomes solving minimal surfaces with zero mean curvature.

$$F(r, z) = r - \eta(z) = 0$$

$$\underline{n} = \frac{\nabla F}{|\nabla F|} = \frac{e_r - \eta_z e_z}{(1 + \eta_z^2)^{1/2}}$$

$$K = \nabla \cdot \underline{n} = \frac{1}{r} \frac{\partial}{\partial r} (r \cdot n_r) + \frac{\partial}{\partial z} (n_z)$$

$$= \frac{1}{\eta (1 + \eta_z^2)^{3/2}} - \left[\frac{\eta_{zz}}{(1 + \eta_z^2)^{3/2}} - \frac{\eta_z^3 \eta_{zz}}{(1 + \eta_z^2)^{5/2}} \right]$$

$$= \frac{1}{(1 + \eta_z^2)^{3/2}} \left(\frac{1}{\eta} - \frac{\eta_{zz}}{1 + \eta_z^2} \right) = 0$$

We obtain $\boxed{\eta \eta_{zz} = 1 + \eta_z^2}$ for $-\frac{h}{2} \leq z \leq \frac{h}{2}$

Aside

$$\cdot (\eta_z^2)' = 2\eta_z \eta_{zz}$$

$$\cdot (1 + \eta_z^2)^{-3/2} = -(1 + \eta_z^2)^{-5/2} \eta_z \eta_{zz}$$

Typical tricks to reduce the order of ODE for surface tension problems

A trick that is useful here is that $(1 + \eta_z^2)' = 2\eta_z \eta_{zz}$

$$\rightarrow \frac{\eta (1 + \eta_z^2)'}{2\eta_z} = 1 + \eta_z^2 \quad \text{or} \quad \frac{\eta_z}{\eta} = \frac{(1 + \eta_z^2)'}{2(1 + \eta_z^2)}$$

We then have $\ln \eta = \frac{1}{2} \ln (1 + \eta_z^2) + C$, which can be rewritten as

$$\eta = C (1 + \eta_z^2)^{1/2} \rightarrow \eta_z = \frac{\sqrt{\eta^2 - C^2}}{C} = \frac{d\eta}{dz} \rightarrow dz = \frac{C}{\sqrt{\eta^2 - C^2}} d\eta$$

$$\rightarrow \left[C \cosh^{-1} \left(\frac{\eta}{C} \right) \right]'$$

The solution reads $z - z_0 = C \cosh^{-1} \left(\frac{\eta}{C} \right)$, or

$$\eta = C \cosh \left(\frac{z - z_0}{C} \right).$$

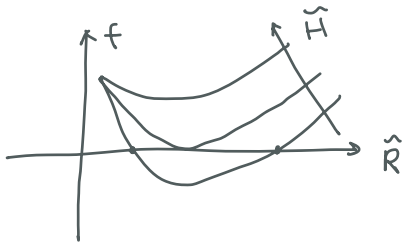
Use boundary conditions to determine integration constants C & z_0 .

Symmetry at $z=0$, $y'_z=0 \rightarrow z_0=0$

Fixed edge at $z=\frac{h}{2}$, $y(\frac{h}{2})=R \rightarrow R=C \cosh(\frac{h}{2c})$

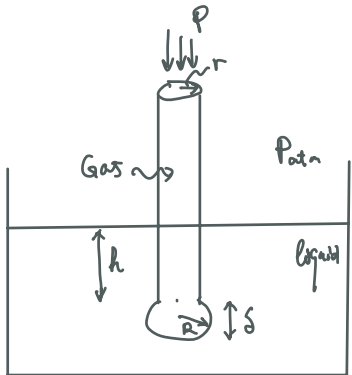
Therefore, the solution is $y=C \cosh(\frac{z}{c})$, where C satisfies $R=C \cosh(\frac{h}{2c})$.
 ↑
 Catenary curve.

Let $\tilde{R}=R/c$, $\tilde{H}=h/R$. Then seek solution $f(\tilde{R}, \tilde{H})=C \cosh(\frac{1}{2}\tilde{H}\tilde{R}) - \tilde{R} = 0$

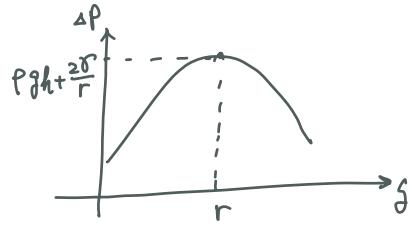


- This equation has two solutions for C when h is not too greater than R : one is for minimal surface and the other is for maximal surface.
- When $\tilde{H} = 1.33$, i.e., $h = 1.33 R$, the two solutions are identical. For $h > 1.33 R$, no solutions (soap film bursts).

• Maximal pressure of a bubble (E. Schrödinger one of pioneers)



$$p = p_{atm} + \rho g h + \frac{2\sigma}{R}$$



$h \gg r \rightarrow$ bubble is approximately spherical

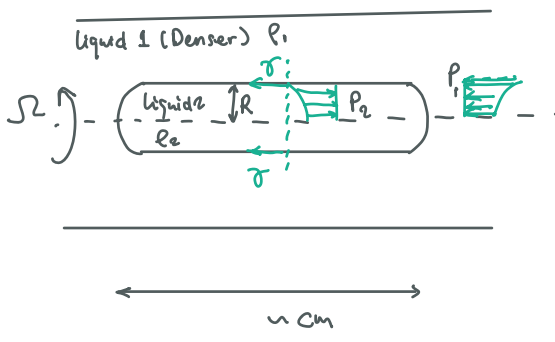
Precise and robust - works even at very high temperatures, allowing experiments

with metals and molten glass. And bubble breaking will "refresh" the interface.

↑
Preventing from potential contaminants

Spinnig drops

Force balance method.



$$\int_0^R 2\pi P_2 r dr = \int_0^R 2\pi P_1 r dr + 2\pi R \sigma$$

$\begin{array}{c} \downarrow \downarrow \downarrow \downarrow P+dP \\ \uparrow \uparrow \uparrow \uparrow P \end{array} \uparrow F_c \sim \text{Centrifugal force}$
 $\longrightarrow dr$

$$\rho dV \frac{U_0^2}{r} = dp \cdot dA \rightarrow \frac{dp}{dr} = \rho \omega^2 r$$

$U_0 = \omega r$

We then have $P_i = C_i + \frac{1}{2} \rho_i \omega^2 r^2$ with C_1, C_2 two unknown integration constants.

① At $r=R$, we know $P_2 - P_1 = \frac{\sigma}{R}$

$$P_1(R) = C_1 + \frac{1}{2} \rho_1 \omega^2 R^2$$

$$P_2(R) = C_2 + \frac{1}{2} \rho_2 \omega^2 R^2$$

$$\rightarrow C_2 - C_1 = \frac{1}{2} (\rho_2 - \rho_1) \omega^2 R^2 + \frac{\sigma}{R}$$

② Horizontal force balance

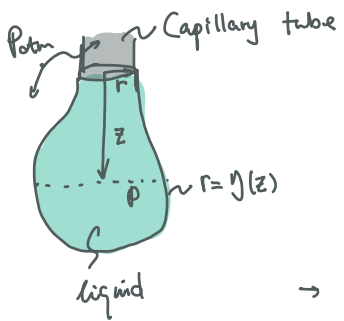
$$\pi R^2 \cdot C_2 + \frac{\pi}{4} \rho_2 \omega^2 R^4 = \pi R^2 \cdot C_1 + \frac{\pi}{4} \rho_1 \omega^2 R^4 + 2\pi R \sigma$$

$$\rightarrow C_2 - C_1 = \frac{1}{4} (\rho_1 - \rho_2) \omega^2 R^2 + \frac{2\sigma}{R}$$

$$\Rightarrow \sigma = \frac{1}{4} (\rho_1 - \rho_2) \omega^2 R^3$$

* A great advantage: It Does not involve contact with a solid.

• Pendant drops



$$P(z) = P_{atm} + \rho g z$$

$$P(z) = P_{atm} + \gamma \cdot \nabla n$$

$$\rightarrow \gamma \cdot \nabla n - \rho g z = 0, \text{ where } \nabla n = -\frac{\int_{z_0}^z}{(1 + r_z^2)^{3/2}} + \frac{1}{r(1 + r_z^2)^{1/2}}$$

Strategy: Solving ODE numerically and using γ as a fitting parameter to match experimental results. The error is within 1%.

Note: When the drop's weight exceeds the capillary force acting on the edge of the tube $2\pi R\gamma$, drop drops!

$$2\pi R\gamma = \alpha \frac{4}{3}\pi R_g^3 \times \rho g$$

\swarrow $\sim 6\% \rightarrow 40\%$ remainder on the tube
 \uparrow


$$\rightarrow R_g = \left(\frac{3}{2\alpha} R l_c^2\right)^{1/3} \sim \text{millimeter scale.}$$

• Stability of pendant drop

Note that previous discussions are all about $\delta F = 0$. This gives extrema but does not specify whether it is a minimum or a maximum. In the problem of soap film between two rings, we

have realized that both could be solved as solutions but one of the two appears to be a maximum - which is unstable. Similar scenarios occur also in the pendant drop problem.

First, consider a simplified model problem - a cylinder



Gravitational E. Surface energy

$$F_V = -\rho g V \times \frac{1}{2} l + \sigma (\pi R^2 + 2\pi R l) + (\sigma_{SL} - \sigma_{SV}) \pi R^2$$

R, l are not independent - They satisfy $\pi R^2 l = V$

Let us rewrite $F_V(R, l)$ as $F(l, V)$

$$F = -\frac{1}{2} \rho g V l + \underbrace{(\sigma + \sigma_{SL} - \sigma_{SV})}_{\sigma(1 - \cos\theta)} \frac{V}{l} + \sigma (4\pi V l)^{1/2}$$

Without loss, let us try $\theta = \pi/2$ and rescale F by $\sigma V^{2/3}$ and l by $V^{1/3}$, say

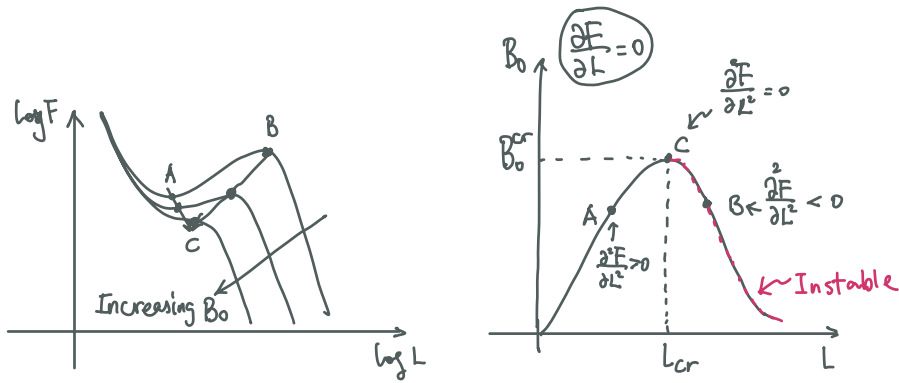
$$F = F/\sigma V^{2/3}, \quad L = l/V^{1/3}, \quad l_c = (\sigma/\rho g)^{1/2}, \quad B_0 = \left(\frac{V^{1/3}}{l_c}\right)^2$$

We now have

$$F = -\frac{1}{2} \left(\frac{V^{1/3}}{l_c}\right)^2 L + \frac{1}{L} + (4\pi)^{1/2} L^{1/2}$$

$$\text{Indeed, } \frac{\partial^2 F}{\partial L^2} \Big|_{L_{cr}} = 0 \text{ gives } \frac{2}{L_{cr}^3} - \frac{\pi^{1/2}}{2L_{cr}^{3/2}} = 0 \rightarrow L_{cr} = \left(\frac{16}{\pi}\right)^{1/3} \quad (*)$$

$$\text{At this moment, } \frac{\partial F}{\partial L} \Big|_{L_{cr}} = 0 \text{ gives } -\frac{1}{2} B_0^{cr} - \frac{1}{L_{cr}^2} + \left(\frac{\pi}{L_{cr}}\right)^{1/2} = 0 \rightarrow B_0^{cr} = \frac{3}{2} \left(\frac{\pi}{2}\right)^{2/3}$$



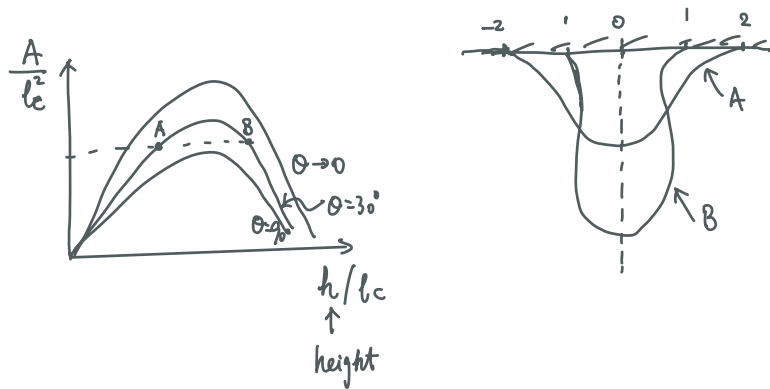
$$\Rightarrow V_{cr} = (B_0^{cr})^{3/2} l_c^3 \approx 2.89 \left(\frac{\sigma}{\rho g}\right)^{3/2} \quad \text{Critical volume}$$

$$l_{cr} = V_{cr}^{1/3} l_c \approx 1.42 \left(\frac{\sigma}{\rho g}\right)^{1/2} \quad \text{Critical height}$$

$$R_{cr} = (V_{cr}/\pi l_{cr})^{1/2} \approx 0.80 \left(\frac{\sigma}{\rho g}\right)^{1/2} \quad \text{Critical radius}$$

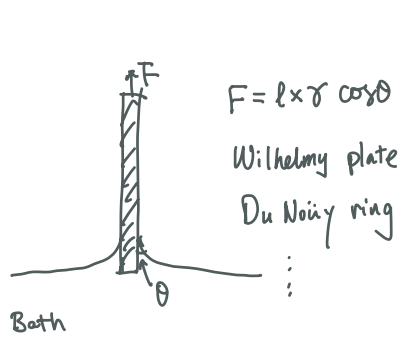
Formal analysis was provided by E. Pitts, JFM (1973) & (1974)

- In JFM 1973 paper, a 2D case was analyzed

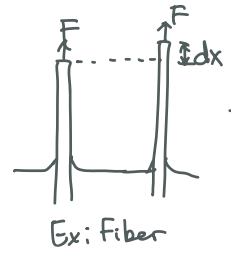


- In JFM 1974 paper, an axisymmetric case was considered.

Force measurements



$F = l \times \gamma \cos \theta$
 Wilhelmy plate
 Du Noüy ring
 ...



$F dx = 2\pi R dx (\gamma_{sv} - \gamma_{sl})$
 $= 2\pi R \gamma \cos \theta$
 $\rightarrow L_{fiber} = 2\pi R$

How to eliminate θ so that $F = l \times \gamma$

① Using a solid with high surface energy - wettable by all usual liquids ($\theta = 0$)

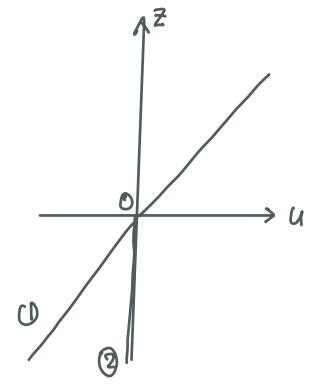
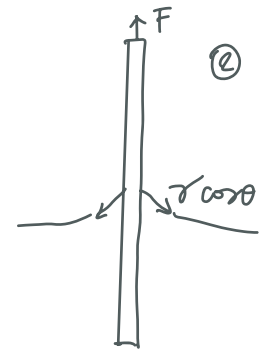
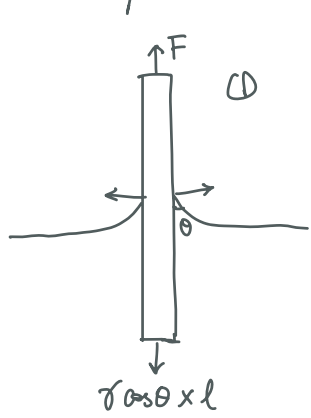
Contaminants that are spontaneously absorbed on the surface would lower the γ_{solid} .

• Platinum - surface can regenerate by a flame.

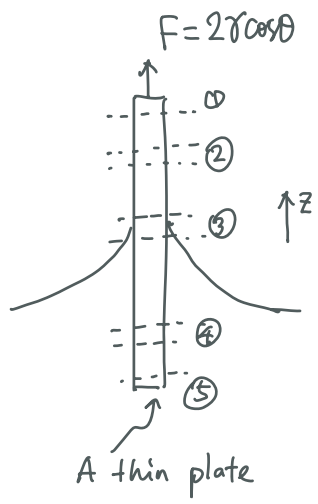
② Quasi-static loading. $F_{max} = l \times \gamma \rightarrow$

Stresses in slender, soft solids

What is the consequence of this $\gamma \cos \theta$? - Need some thought



Need to consider the boundary value problem, which can be derived via variational analysis. But here I decided to use the method of force/stress balance.



Governing equations:

②: $\sigma + d\sigma$ (up arrow) and σ (down arrow)

$$\frac{d\sigma}{dz} = 0 \rightarrow \sigma \equiv \sigma^+, z > 0$$

④: $\sigma \equiv \sigma^-, z < 0$

Boundary conditions:

①: $\sigma^+ t = F - 2\gamma_{sv} \rightarrow \sigma^+ = \frac{2\gamma \cos\theta - 2\gamma_{sv}}{t}$

③: $\sigma^- t = \sigma^+ t + \underbrace{2\gamma_{sv} - 2\gamma \cos\theta - 2\gamma_{sl}}_{=0} \rightarrow \sigma^- = \sigma^+$

⑤: $\sigma^- = \frac{-2\gamma_{sl}}{t} (= \sigma^+ \checkmark)$

Does not depend on shape, say

$$\sigma = -\frac{t}{2} \frac{P_i - P_o}{P_o} = -\frac{\gamma_{sl}}{t/2}$$

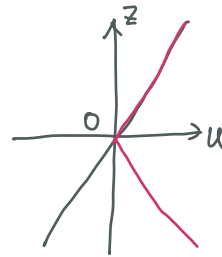
This means there's no stress jump if all γ 's are constant!!!

Since measures are made relative to $\sigma_0 = -2\gamma_{sr}$, we expect (46)

that

$$\sigma_{Exp}^+ = \sigma_{Exp}^- = \frac{2\gamma \cos\theta}{t}$$

or



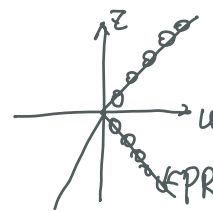
$$\frac{du}{dz} = \epsilon_z = \frac{2\gamma \cos\theta}{Et}$$

However, experiments by Marchand et al. PRL (2012) on small fibers showed the red curve, which needs further verification via plate experiments!

$$\sigma_{zz} = \begin{cases} \frac{2\gamma \cos\theta}{R} - \frac{2\gamma_{sr}}{R}, & z > 0 \\ -\frac{2\gamma_{sl}}{R}, & z < 0 \end{cases} \quad \sigma_{\theta\theta} = \sigma_{rr} = \begin{cases} -\frac{\gamma_{sr}}{R}, & z > 0 \\ -\frac{\gamma_{sl}}{R}, & z < 0 \end{cases}$$

$$\Rightarrow \sigma_{zz}^{Exp} = \frac{2\gamma \cos\theta}{R}, \quad \sigma_{\theta\theta}^{Exp} = \sigma_{rr}^{Exp} = \begin{cases} 0, & z > 0 \\ \frac{\gamma \cos\theta}{R}, & z < 0 \end{cases}$$

$$\Rightarrow \epsilon_{zz} = \frac{\sigma_{zz} - \nu(\sigma_{rr} + \sigma_{\theta\theta})}{E} = \begin{cases} \frac{2\gamma \cos\theta}{R} \\ \frac{\gamma \cos\theta}{R} \end{cases}$$



PRL (2012). why?

Stresses in soft thin sheets

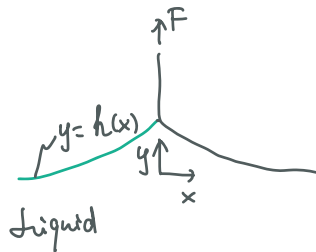
A recent work by Kumar et al. Nat. Mater. (2020) did use a thin plate/sheet.

However, the stress/strain field are not directly measured.

The question posed by this work is which boundary condition to use. (47)



The experimental set-up goes as following



• For liquid surface

$$\gamma \nabla \cdot \underline{n} + \rho g h = 0, \quad \nabla \cdot \underline{n} = -\frac{h_{xx}}{(1+h_x^2)^{3/2}}$$

Subject to $h(\infty) = 0, h(0) = \delta$ (prescribed)

$$F = \gamma + \gamma_{sv} - \gamma_{sl} \\ = \gamma(1 + \cos\theta)$$

• For thin sheet on liquid surface

$$\gamma \nabla \cdot \underline{n} + \rho g h = 0, \quad h(\infty) = 0, h(0) = \delta.$$

Then it is found that the two profiles are identical, regardless of the liquid used.

$$\Rightarrow \gamma = \gamma, \text{ i.e. } \leftarrow \gamma \rightarrow \gamma \text{ (B)}$$

However, if we go through the variation, the true governing equation should be

$$(\gamma_v + \gamma_{sl} + \gamma_{sv}) \nabla \cdot \underline{n} + \rho g h = 0$$

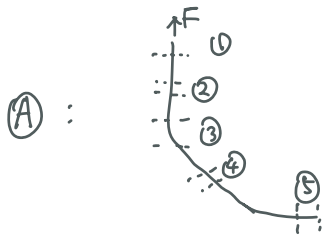
subject to (A) $\gamma_v + \gamma_{sl} + \gamma_{sv} = \gamma$. Let $\gamma = \gamma_v + \gamma_{sl} + \gamma_{sv}$, leading to the

same results. \rightarrow Both (A) & (B) can be used, but should be cautious about

the reference state! The question of (A) or (B) is not answered!

A possible way to address this problem could be given by examining the $\gamma(x)$!

in the sheet.

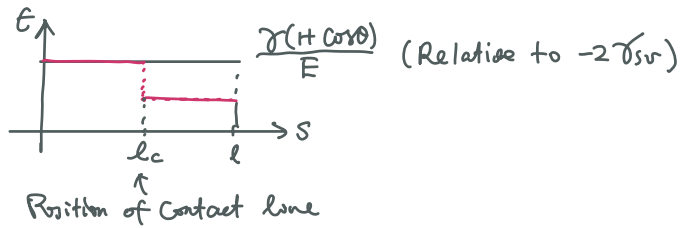


(2) - (4) $\begin{matrix} \uparrow N+dN \\ \downarrow N \end{matrix} \rightarrow N=C$

(1) $\begin{matrix} \uparrow F \\ \downarrow \delta_{sv} \\ \downarrow N \end{matrix} \quad N^+ = F - 2\delta_{sv} = \gamma - \delta_{sv} - \delta_{sl}$

(3) $\begin{matrix} \uparrow N^+ \\ \downarrow \delta_{sv} \\ \downarrow N^- \\ \downarrow \delta_{sl} \end{matrix} \quad N^- = N^+$

(5) $\begin{matrix} \leftarrow \delta_{sv} \\ \leftarrow N^- \\ \leftarrow \delta_{sl} \end{matrix} \rightarrow \gamma \quad N^- = \gamma - \delta_{sv} - \delta_{sl} \checkmark$



(B) would give a jump in E , shown as the red curve.